

MODIFICATION OF THE LS-STAG IMMERSED BOUNDARY METHOD FOR SIMULATING TURBULENT FLOWS

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Abstract

We constructed the LS-STAG discretisation for 2D Reynolds-averaged Navier — Stokes equations, filtered Navier — Stokes equations (as used for large eddy simulation and detached eddy simulation) and equations employed in the Smagorinsky, Spalart — Allmaras, $k-\varepsilon$, $k-\omega$ and $k-\omega$ Menter's Shear Stress Transport turbulence models. We added a fourth grid to the LS-STAG mesh consisting of three staggered grids. We computed the following parameters at the centres of the additional mesh cells: turbulent shear stress and, depending on the turbulence model used, turbulence kinetic energy, turbulent viscosity, and turbulent kinetic energy dissipation rate. We verified the developed numerical method by solving the problem of flow around a circular airfoil when the flow has a high Reynolds number ($10^2 \dots 10^7$). The obtained results are in good agreement with published experimental data and numerical results of other researchers. Our modification of the LS-STAG immersed boundary method made it possible to model the so-called "drag crisis" phenomenon for a circular airfoil when $Re = 10^5 \dots 10^6$

Keywords

Immersed boundary method, LS-STAG method, turbulence models, Reynolds-averaged Navier — Stokes equations, large eddy simulation, detached eddy simulation, airfoil

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Introduction. In number of engineering applications, for example in flow simulation around wind turbine rotors, heat exchanger pipes, overhead and underwater cables and pipes, building structures, marine infrastructure elements, etc., it is necessary to solve coupled hydroelastic problems. Such problems are enough difficult for the numerical solution and require high-precision numerical methods usage. There is a special class of numerical methods — the immersed boundary methods — in which the mesh is not connected to the body boundary and is not modified during the entire computation, despite the immersed body movement [1]. These methods involve the rectangular meshes usage. Cells of irregular shape, called the "cut-cells", are formed at the intersection of a rectangular mesh with the immersed boundary. One of the most effective methods in this class is the LS-STAG method [2]. This method has not been implemented in both commercial and free software packages.

To obtain accurate quantitative results when simulating unsteady flows characterized by high-speed airfoils movement, and hence by high values of local Reynolds number, strong mesh refinement is need. It leads to a sharp increase in computational cost of direct numerical simulation. The traditional way here is turbulence simulation by using some well-known approaches and turbulence models. However, the corresponding numerical schemes haven't been developed for LS-STAG approach.

In the present research the LS-STAG discretizations for two-dimensional RANS, LES and DES equations and transport equations from Smagorinsky, Spalart — Allmaras, $k-\varepsilon$, $k-\omega$ and $k-\omega$ SST turbulence models are constructed.

Governing equations. The problem is considered for 2D unsteady case when the flow around an airfoil assumed to be viscous and incompressible within the framework of RANS, LES and DES approaches. In contrast to direct numerical simulation (DNS) based on solution of Navier — Stokes equations and resolution of all turbulent movement scales, turbulence models usage involves simulation of turbulence scales contribution to the averaged motion (in case of RANS approach) or simulation of scales that do not exceed the filter width Δ (in case of LES approach). In case of RANS approach one speaks of the Reynolds stress simulation and in case of LES approach one speaks of the subgrid stress simulation.

The Reynolds-averaged Navier — Stokes equations are being solved in RANS approach, and the filtered Navier — Stokes equations are being solved in LES approach instead of the Navier — Stokes equations. DES approach usage means that RANS equations are being solved in one part of the computational domain, and LES equations are solved in the other part. It is possible to write down the unified governing equations in dimensionless variables for all approaches, because the form of LES equations is similar to the form of RANS equations. So the incompressible flow is described by the following RANS/LES/DES equations:

$$\nabla \cdot \mathbf{v} = 0, \quad \frac{\partial \mathbf{v}}{\partial t} + (\mathbf{v} \cdot \nabla) \mathbf{v} = -\nabla p + \nu \Delta \mathbf{v} + \nabla \cdot \hat{\tau}^t. \quad (1)$$

Here $\mathbf{v} = \mathbf{v}(x, y, t) = u \cdot \mathbf{e}_x + v \cdot \mathbf{e}_y$ is the dimensionless Reynolds averaged of filtrated velocity, $p = p(x, y, t)$ is the dimensionless Reynolds averaged of filtrated pressure, $\nu = 1/\text{Re}$ is the dimensionless viscosity, $\hat{\tau}^t$ is the Reynolds or subgrid stresses tensor. The relationship between $\hat{\tau}^t$ and flow Reynolds averaged or filtrated variables is given by the turbulence model.

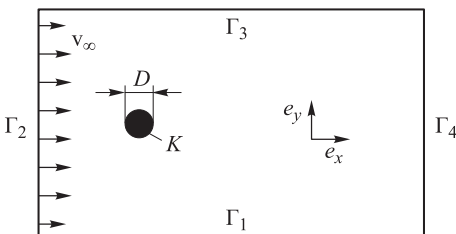


Fig. 1. Computational domain

Flow around a fixed airfoil in computational domain Ω with boundary $\Gamma = \Gamma_1 \cup \Gamma_2 \cup \Gamma_3 \cup \Gamma_4$ is considered (Fig. 1). In all our simulations, the upstream and outflow boundaries are set at the distances $8D$ and $15D$, respectively, from the airfoil center, and the blockage ratio is equal to $1/12$. The previous studies have shown that such computational domain is sufficiently

wide to obtain results that are don't depend on the domain size.

We denote the airfoil boundary as K . Then the boundary conditions are the following:

$$\mathbf{v} |_{\Gamma_1 \cup \Gamma_2 \cup \Gamma_3} = \mathbf{v}_\infty, \quad \frac{\partial \mathbf{v}}{\partial \mathbf{n}} |_{\Gamma_4} = 0, \quad \mathbf{v} |_K = \mathbf{v}^{ib}.$$

It is possible to distinguish the linear turbulence scale $l_{turb} = l_{turb}(\mathbf{r})$ for all turbulence models. In the framework of RANS approach this scale l_{turb} is equal to scale $l_{RANS} = l_{RANS}(\mathbf{r})$, which is determined by the turbulence model (Table 1).

Table 1

Turbulence scale l_{RANS} for some turbulence models [3]

Turbulence model	l_{RANS}	Comments
Spalart — Allmaras [4]	d_w	d_w is the distance between the field point and the nearest wall
$k - \varepsilon$ [5]	$k^{3/2} \varepsilon^{-1}$	ε is the dissipation rate of the turbulent kinetic energy k
$k - \omega$ [6], $k - \omega$ SST [7]	$k^{1/2} (\beta^* \omega)^{-1}$	ω is the specific dissipation rate of the k , $\beta^* = 0.09$

In case of LES approach, the scale l_{turb} is equal to subgrid scale:

$$l_{LES} = C_{LES} \Delta. \tag{2}$$

Here $\Delta = \Delta(\mathbf{r})$ is the characteristic filter size at the point of computational domain with the radius vector \mathbf{r} , and C_{LES} is the empirical constant, which choice depends on the turbulence model and numerical method used to solve the problem (1) in the whole. Within the DES approach the linear turbulence scale l_{turb} is equal to hybrid linear scale

$$l_{DES} = \min\{l_{RANS}, C_{DES} \Delta\}. \tag{3}$$

Here C_{DES} is the empirical constant similar to C_{LES} , and the maximum of the mesh steps at the point of computational domain with the radius vector \mathbf{r} is used as the characteristic filter size $\Delta = \Delta(\mathbf{r})$. Thus, DES operates as RANS in the domain where the mesh is too coarse and not suitable for resolving turbulent structures, i. e. at $C_{DES} \Delta > l_{RANS}$, and DES operates as subgrid model for LES in the domain where the grid is sufficiently fine [3]. It should be noted that Smagorinsky [3] model is used only within LES approach.

In this paper Eddy Viscosity turbulence models (EVM) are considered. In EVM models the eddy viscosity ν^t (and the turbulent kinetic energy k in case of two-equation models) is simulated and Reynolds or subgrid stresses are evaluated using the Boussinesq eddy viscosity assumption [3]:

$$\tau_{xx}^t = 2\nu^t \frac{\partial u}{\partial x} + \frac{2}{3} k; \quad \tau_{yy}^t = 2\nu^t \frac{\partial v}{\partial y} + \frac{2}{3} k; \tag{4}$$

$$\tau_{xy}^t = v^t \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right). \quad (5)$$

Here τ_{xx}^t and τ_{yy}^t are normal Reynolds or subgrid stresses and τ_{xy}^t is shear Reynolds or subgrid stress. In cases of algebraic turbulence models or models with one differential equation the turbulent kinetic energy is assumed to be zero and only eddy viscosity value is computed. For example, in the Smagorinsky model [8] the eddy viscosity is defined by the following formula:

$$v^t = (C_S \Delta)^2 \sqrt{2 \left\{ \left(\frac{\partial u}{\partial x} \right)^2 + \left(\frac{\partial v}{\partial y} \right)^2 \right\} + \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right)^2}. \quad (6)$$

Here C_S is the empirical constant (the Smagorinsky constant). Choice of the C_S value depends on the numerical method used to solve the problem, because at LES approach the accuracy of large-scale vortex structures resolution depends not only on the mesh, but also on numerical method properties, in particular, numerical dissipation. If the numerical dissipation is large, it is necessary to choose smaller values of C_S , and if numerical dissipation is small, the C_S value should be chosen larger.

For EVM with differential equations the governing equations, initial and boundary conditions are given by the turbulence model. In the most general way, they may be written as the following:

$$\begin{aligned} \frac{\partial \psi}{\partial t} + (\mathbf{v} \cdot \nabla) \psi &= \text{Prod} - \text{Dis} + \nabla \cdot [(\mathbf{v} + \Gamma_\psi) \nabla \psi] + \text{Add}; \\ \psi(\mathbf{r}, 0) &= \psi_0(\mathbf{r}), \quad \psi|_{\Gamma_1 \cup \Gamma_2 \cup \Gamma_3} = \psi_\infty, \quad \psi|_K = \psi^{ib}, \quad \left. \frac{\partial \psi}{\partial \mathbf{n}} \right|_{\Gamma_4} = 0. \end{aligned} \quad (7)$$

Here Prod is the production term which describes the generation of Reynolds or subgrid stresses; Dis is the destruction term; Add is the additional term; ψ and Γ_ψ are given by the particular turbulence model (Table 2).

Table 2

Itemization of symbols in (7) and rules for v^t computation for some turbulence models [3]

Term	Spalart — Allmaras	$k - \varepsilon$		$k - \omega$		$k - \omega$ SST	
Ψ	\tilde{v}	k	ε	k	ω	k	ω
Add	0	0	0	0	0	0	$(1 - F_1) D_{k\omega}$
Prod	P^v	P^τ	$\frac{1.44 \varepsilon P^\tau}{k}$	P^τ	$\frac{5\omega P^\tau}{9k}$	P^τ	$\frac{(0.44 + 0.11 F_1) P^\tau}{v^t}$
Dis	D^v	$\frac{k^{3/2}}{l_{turb}}$	$\frac{1.92 \varepsilon^2}{k}$	$\frac{k^{3/2}}{l_{turb}}$	$\frac{3\omega^2}{40}$	$k^{3/2} / l_{turb}$	$0.0828 - 0.0078 F_1$
Γ_ψ	\tilde{v}	v^t	$v^t / 1.3$	$v^t / 2$	$v^t / 2$	$(1 - 0.5 F_1) v^t$	$(0.856 - 0.356 F_1) v^t$
v^t	$\tilde{v} f_{v1}$	$0.09 k^2 / \varepsilon$		k / ω		$0.31 k / G_1$	

The following designations are introduced in Table 2: $\tilde{\nu}$ is the Spalart — Allmaras (S-A) working variable [4]; ε is the dissipation rate of the turbulent kinetic energy k ; ω is the specific dissipation rate of k ;

$$F_1 = \tanh \left(\left[\left[\min \left(\max \left\{ \frac{\sqrt{k}}{0.09\omega d_w}, \frac{500\nu}{d_w^2\omega} \right\}, \frac{3.424k}{CD_{k\omega}d_w^2} \right) \right] \right]^4 \right);$$

$$CD_{k\omega} = \max(D_{k\omega}, 10^{-20}); \quad D_{k\omega} = \frac{1.712\nabla k \cdot \nabla \omega}{\omega};$$

$$P^v = 0.1355[1 - f_{t2}]\tilde{S}\tilde{\nu}; \quad f_{t2} = 1.2e^{-0.5\chi^2}; \quad \chi = \frac{\tilde{\nu}}{\nu}; \quad \tilde{S} = \left| \frac{\partial u}{\partial y} - \frac{\partial v}{\partial x} \right| + f_{v2} \frac{\tilde{\nu}}{0.1681l_{turb}^2};$$

$$f_{v2} = 1 - \frac{\chi}{1 + \chi f_{v1}}; \quad f_{v1} = \frac{\chi^3}{\chi^3 + 357.911}; \quad P^r = \tau_{xx}^t \frac{\partial u}{\partial x} + \tau_{yy}^t \frac{\partial v}{\partial y} + \tau_{xy}^t \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right);$$

$$D^v = (3.2391f_w - 0.8061f_{t2}) \left(\frac{\tilde{\nu}}{l_{turb}} \right)^2; \quad f_w = g \left(\frac{65}{g^6 + 64} \right)^{1/6}; \quad g = r + 0.3(r^6 - r);$$

$$r = \min \left(\frac{\tilde{\nu}}{0.1681\tilde{S}l_{turb}^2}, 10 \right); \quad G_1 = \max \left(0.31\omega, \left| \frac{\partial u}{\partial y} - \frac{\partial v}{\partial x} \right| F_2 \right);$$

$$F_2 = \tanh \left[\left\{ \max \left(\frac{2\sqrt{k}}{0.09\omega d_w}, \frac{500\nu}{d_w^2\omega} \right) \right\}^2 \right].$$

Modification of the LS-STAG immersed boundary method. The Cartesian mesh with cells $\Omega_{i,j} = (x_{i-1}, x_i) \times (y_{j-1}, y_j)$ is introduced in the rectangular computational domain Ω . It is denoted that $\Gamma_{i,j}$ is the face of $\Omega_{i,j}$ cell and $\mathbf{x}_{i,j}^c = (x_i^c, y_j^c)$ is the center of this cell, which is called "base mesh". Pressure is computed in the center of $\Omega_{i,j}$. Unknown components $u_{i,j}$ and $v_{i,j}$ of velocity vector \mathbf{v} are computed in the middle of fluid parts of the cell faces. These points are the centers of control volumes $\Omega_{i,j}^u = (x_i^c, x_{i+1}^c) \times (y_{j-1}, y_j)$ (x -mesh) and $\Omega_{i,j}^v = (x_{i-1}, x_i) \times (y_j^c, y_{j+1}^c)$ (y -mesh) with faces $\Gamma_{i,j}^u$ and $\Gamma_{i,j}^v$ and squares M_{ij}^x and M_{ij}^y , respectively (Fig. 2).

The level-set function $\varphi = \varphi(\mathbf{r}) = \varphi(x, y)$ [9] is used for immersed boundary Γ^{ib} description [2]:

$$\begin{aligned} \varphi(\mathbf{r}) < 0, \quad \mathbf{r} \in \Omega^f = \Omega \setminus \{\Omega^{ib} \cup \Gamma^{ib}\}; \\ \varphi(\mathbf{r}) = 0, \quad \mathbf{r} \in \Gamma^{ib}; \\ \varphi(\mathbf{r}) > 0, \quad \mathbf{r} \in \Omega^{ib}. \end{aligned}$$

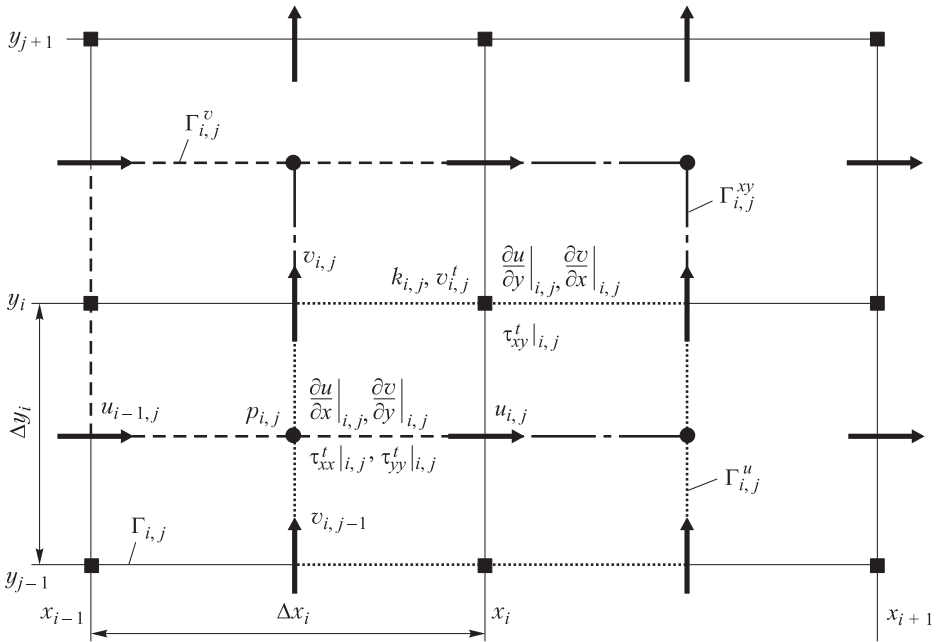


Fig. 2. Staggered arrangement of the variables on the LS-STAG mesh

The boundary Γ^{ib} is represented by a line segment on the cut-cell $\Omega_{i,j}$ (Fig. 3). Location of this segment endpoints is defined by a linear interpolation of the variable $\varphi_{i,j} = \varphi(x_i, y_j)$. The cell-face fraction ratios $\theta_{i,j}^u$ and $\theta_{i,j}^v$ are introduced [2].

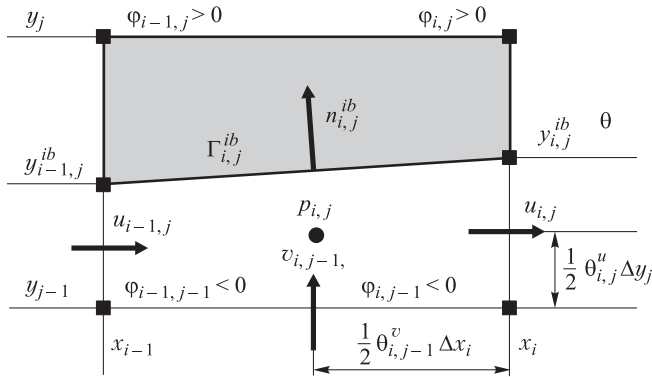


Fig. 3. Example of the cut-cell on the LS-STAG mesh

They take values in interval $[0,1]$ and represent the fluid parts of the east and north faces of $\Gamma_{i,j}$, respectively. The cell-face fraction ratios are defined by a one-dimensional linear interpolations of function $\varphi(x, y)$ in interval $[y_{j-1}, y_j]$ and $\varphi(x, y)$ in interval $[x_{i-1}, x_i]$:

$$\theta_{i,j}^u = \frac{\min(\varphi_{i,j-1}, \varphi_{i,j})}{\min(\varphi_{i,j-1}, \varphi_{i,j}) - \max(\varphi_{i,j-1}, \varphi_{i,j})}; \quad \theta_{i,j}^v = \frac{\min(\varphi_{i-1,j}, \varphi_{i,j})}{\min(\varphi_{i-1,j}, \varphi_{i,j}) - \max(\varphi_{i-1,j}, \varphi_{i,j})}.$$

In 2D case, the cut-cells can be classified into trapezoidal, triangular and pentagonal cells. Examples of each type cut-cells are shown on Fig. 4.

To preserve the five-point structure of the stencil of the MAC method, which can be considered as some kind of "predecessor" of the LS-STAG method, we need to make distinction between the discretization of the normal and shear stresses [2] (Fig. 4). It is conveniently to sample the eddy viscosity ν^t , the turbulent kinetic

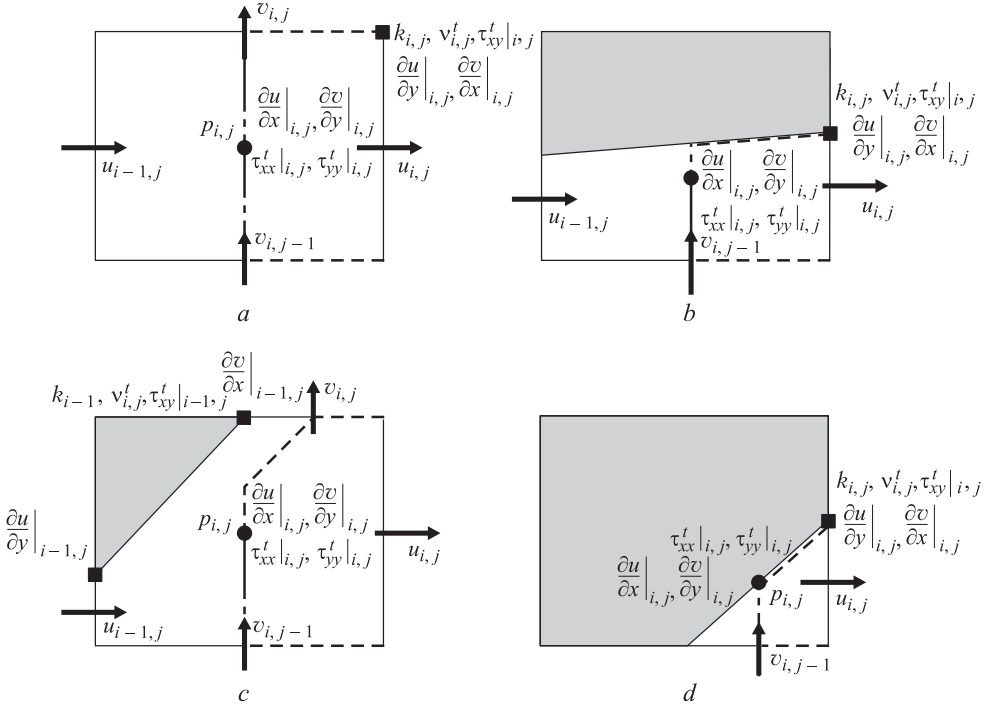


Fig. 4. Location of the variables discretization points in case of base types cells of the LS-STAG mesh:

- a — Cartesian Fluid Cell; b — North Trapezoidal Cell; c — Northwest Pentagonal Cell; d — Northwest Triangle Cell

energy k , the dissipation rate of the kinetic energy, ε and the specific dissipation rate of kinetic energy ω at the same points as the shear stresses. Thus, in case of the LS-STAG method usage for RANS-based models the fourth mesh (xy -mesh) with cells $\Omega_{i,j}^{xy} = (x_i^c, x_{i+1}^c) \times (y_j^c, y_{j+1}^c)$ is needed. The faces of these cells are $\Gamma_{i,j}^{xy}$ (Fig. 2) and their areas are $M_{i,j}^{xy}$. If i and j take values from ranges $1, \dots, N$ and $1, \dots, M$, respectively, the base mesh contains $E = NM$ cells, x -mesh contains $E_x = (N - 1)M$ cells, y -mesh contains $E_y = N(M - 1)$ cells and xy -mesh contains $E_{xy} = (N - 1)(M - 1)$ cells.

It is possible to assign a weight $\alpha_{i,j}$ to each cell $\Omega_{i,j}$ of the base mesh:

$$\alpha_{i,j} = \begin{cases} 0, & \text{if } \Omega_{i,j} \text{ is the solid cell;} \\ 1/3, & \text{if } \Omega_{i,j} \text{ is the triangular cell;} \\ 1/4, & \text{otherwise.} \end{cases}$$

Then $M_{i,j}^{xy}$ can be expressed through the area of base mesh cells:

$$M_{i,j}^{xy} = \alpha_{i,j-1}V_{i,j-1} + \alpha_{i-1,j}V_{i-1,j} + \alpha_{i,j}V_{i,j} + \alpha_{i,j+1}V_{i,j+1}.$$

Here $V_{i,j}$ is the area of the cell $\Omega_{i,j}$.

Since v^t and shear Reynolds or subgrid stresses (5) are sampled at the same points, it follows that

$$\tau_{xy}^t |_{i,j} = v_{i,j}^t \left(\left. \frac{\partial u}{\partial y} \right|_{i,j} + \left. \frac{\partial v}{\partial x} \right|_{i,j} \right), \tag{8}$$

whereas averaged values of turbulent viscosity $\bar{v}_{i,j}^t$ and the turbulent kinetic energy $\bar{k}_{i,j}$ should be used for the computation of the normal Reynolds or subgrid stresses (4):

$$\tau_{xx}^t |_{i,j} = 2\bar{v}_{i,j}^t \left. \frac{\partial u}{\partial x} \right|_{i,j} + \frac{2}{3}\bar{k}_{i,j}; \quad \tau_{yy}^t |_{i,j} = 2\bar{v}_{i,j}^t \left. \frac{\partial v}{\partial y} \right|_{i,j} + \frac{2}{3}\bar{k}_{i,j};$$

$$\bar{v}_{i,j}^t = \alpha_{i,j}(v_{i,j}^t + v_{i,j-1}^t + v_{i-1,j}^t + v_{i-1,j-1}^t); \quad \bar{k}_{i,j} = \alpha_{i,j}(k_{i,j} + k_{i,j-1} + k_{i-1,j} + k_{i-1,j-1}). \tag{9}$$

Formulae for normal stresses $\left. \frac{\partial u}{\partial x} \right|_{i,j}$ and $\left. \frac{\partial v}{\partial y} \right|_{i,j}$ computation are the following:

$$\left. \frac{\partial u}{\partial x} \right|_{i,j} \approx \frac{\theta_{i,j}^u u_{i,j} - \theta_{i-1,j}^u u_{i-1,j} + (\theta_{i-1,j}^u - \theta_{i,j}^u) u_{i,j}^{ib}}{V_{i,j} / \Delta y_j};$$

$$\left. \frac{\partial v}{\partial y} \right|_{i,j} \approx \frac{\theta_{i,j}^v v_{i,j} - \theta_{i,j-1}^v v_{i,j-1} + (\theta_{i,j-1}^v - \theta_{i,j}^v) v_{i,j}^{ib}}{V_{i,j} / \Delta x_i}.$$

formulae for shear stresses $\left. \frac{\partial u}{\partial y} \right|_{i,j}$ and $\left. \frac{\partial v}{\partial x} \right|_{i,j}$ computation depend on the type of $\Omega_{i,j}^{xy}$ cell:

$$\left. \frac{\partial u}{\partial y} \right|_{i,j} \approx \begin{cases} \frac{u_{i,j+1} - u_{i,j}}{(\theta_{i,j+1}^u \Delta y_{j+1} + \theta_{i,j}^u \Delta y_j) / 2}, & \text{if } \theta_{i,j}^u \neq 0, \theta_{i,j+1}^u \neq 0; \\ \left. \frac{\partial u}{\partial y} \right|_{i,j}^{ib,s} = \frac{u_{i,j+1} - u(x_i, y_{i,j+1}^{ib})}{\theta_{i,j+1}^u \Delta y_{j+1} / 2}, & \text{if } \theta_{i,j}^u = 0, \theta_{i,j+1}^u \neq 0; \\ \left. \frac{\partial u}{\partial y} \right|_{i,j}^{ib,n} = \frac{u(x_i, y_{i,j}^{ib}) - u_{i,j}}{\theta_{i,j}^u \Delta y_j / 2}, & \text{if } \theta_{i,j}^u \neq 0, \theta_{i,j+1}^u = 0; \end{cases}$$

$$\frac{\partial v}{\partial x} \Big|_{i,j} \approx \begin{cases} \frac{v_{i+1,j} - v_{i,j}}{(\theta_{i+1,j}^v \Delta x_{i+1} + \theta_{i,j}^v \Delta x_i) / 2}, & \text{if } \theta_{i,j}^v \neq 0, \theta_{i+1,j}^v \neq 0; \\ \frac{\partial v}{\partial x} \Big|_{i,j}^{ib,w} = \frac{v_{i+1,j} - v(x_{i+1,j}^{ib}, y_j)}{\theta_{i+1,j}^v \Delta x_{i+1} / 2}, & \text{if } \theta_{i,j}^v = 0, \theta_{i+1,j}^v \neq 0; \\ \frac{\partial v}{\partial x} \Big|_{i,j}^{ib,e} = \frac{v(x_{i,j}^{ib}, y_j) - v_{i,j}}{\theta_{i,j}^v \Delta x_i / 2}, & \text{if } \theta_{i,j}^v \neq 0, \theta_{i+1,j}^v = 0. \end{cases}$$

Components of hydrodynamic force acting on the immersed boundary can be computed as the following:

$$F_{xa} = \sum_{\text{cut-cells } \Omega_{i,j}^{ib}} (\theta_{i-1,j}^u - \theta_{i,j}^u) \Delta y_j \left(p_{i,j} - v \frac{\partial u}{\partial x} \Big|_{i,j} \right) - v \text{Quad}_{i,j}^{ib} \left(\frac{\partial u}{\partial y} \mathbf{e}_y \cdot \mathbf{n} \right);$$

$$F_{ya} = \sum_{\text{cut-cells } \Omega_{i,j}^{ib}} -v \text{Quad}_{i,j}^{ib} \left(\frac{\partial v}{\partial x} \mathbf{e}_x \cdot \mathbf{n} \right) + (\theta_{i,j-1}^v - \theta_{i,j}^v) \Delta x_i \left(p_{i,j} - v \frac{\partial v}{\partial y} \Big|_{i,j} \right).$$

Here F_{xa} is the drag force, F_{ya} is the lift force, $\Delta x_i = x_i - x_{i-1}$, $\Delta y_j = y_j - y_{j-1}$, $\text{Quad}_{i,j}^{ib}$ is the quadrature of the shear stresses. $\text{Quad}_{i,j}^{ib}$ has to be adapted to each type of cut-cells. This quadrature is based on the location of point where the shear stresses are sampled in Fig. 4 and the trapezoidal rule.

It is conveniently to sample the linear turbulence scale l_{turb} and the characteristic filter size Δ for LES and DES at the same points as the v^t and k . We recall that the maximum mesh step at the given point of the computational domain is used as a filter size Δ for DES approach. Since we deal with xy -mesh, the characteristic filter size is defined as a following:

$$\Delta_{i,j} = \Delta_{i,j}^{\max} = \max\{\Delta y_{i-1,j}^{xy}, \Delta y_{i,j}^{xy}, \Delta y_{i+1,j}^{xy}, \Delta x_{i,j-1}^{xy}, \Delta x_{i,j}^{xy}, \Delta x_{i,j+1}^{xy}\},$$

where

$$\Delta y_{i,j}^{xy} = \frac{1}{2} (\theta_{i,j}^u \Delta y_j + \theta_{i,j+1}^u \Delta y_{j+1}); \quad \Delta x_{i,j}^{xy} = \frac{1}{2} (\theta_{i,j}^v \Delta x_i + \theta_{i+1,j}^v \Delta x_{i+1}).$$

Within LES approach the following filter can also be used on the LS-STAG mesh:

$$\Delta_{i,j} = \Delta_{i,j}^{vol} = \sqrt{M_{i,j}^{xy}}.$$

According to the concept of the LS-STAG method, equations (1), (7) should be written in integral form for cell of base mesh, cell of x -mesh, cell of y -mesh and cell of xy -mesh, respectively:

$$\int_{\Gamma_{i,j}} \mathbf{v} \cdot \mathbf{n} dS = 0; \tag{10}$$

$$\begin{aligned} \frac{d}{dt} \int_{\Omega_{i,j}^u} u dV + \int_{\Gamma_{i,j}^u} (\mathbf{v} \cdot \mathbf{n}) u dS + \int_{\Gamma_{i,j}^u} p \mathbf{e}_x \cdot \mathbf{n} dS - \int_{\Gamma_{i,j}^u} \mathbf{v} \nabla u \cdot \mathbf{n} dS - \\ - \int_{\Gamma_{i,j}^u} \tau_{xx}^t \mathbf{e}_x \cdot \mathbf{n} dS - \int_{\Gamma_{i,j}^u} \tau_{xy}^t \mathbf{e}_y \cdot \mathbf{n} dS = 0; \end{aligned} \quad (10)$$

$$\begin{aligned} \frac{d}{dt} \int_{\Omega_{i,j}^v} v dV + \int_{\Gamma_{i,j}^v} (\mathbf{v} \cdot \mathbf{n}) v dS + \int_{\Gamma_{i,j}^v} p \mathbf{e}_y \cdot \mathbf{n} dS - \int_{\Gamma_{i,j}^v} \mathbf{v} \nabla v \cdot \mathbf{n} dS - \\ - \int_{\Gamma_{i,j}^v} \tau_{yy}^t \mathbf{e}_y \cdot \mathbf{n} dS - \int_{\Gamma_{i,j}^v} \tau_{xy}^t \mathbf{e}_x \cdot \mathbf{n} dS = 0; \end{aligned}$$

$$\frac{d}{dt} \int_{\Omega_{i,j}^{xy}} \psi dV + \int_{\Gamma_{i,j}^{xy}} (\mathbf{v} \cdot \mathbf{n}) \psi dS = \int_{\Gamma_{i,j}^{xy}} (\mathbf{v} + \Gamma_\psi) (\nabla \psi \cdot \mathbf{n}) dS + \int_{\Omega_{i,j}^{xy}} (\text{Prod} - \text{Dis} + \text{Add}) dV. \quad (11)$$

In case of fixed immersed boundaries by analogy with the LS-STAG discretization of Navier — Stokes equations [2] the general form of the LS-STAG discretization for (10), (11) can be written as the following:

$$D^x U_x + D^y U_y + \bar{U}^{ib} = 0;$$

$$\frac{d}{dt} (M^x U_x) + C^x U_x + G^x (P - T_{xx}) - D_x^t T_{xy} - \nu K^x U_x + S_x^{ib,c} - \nu S_x^{ib,\nu} = 0; \quad (12)$$

$$\frac{d}{dt} (M^y U_y) + C^y U_y + G^y (P - T_{yy}) - D_y^t T_{xy} - \nu K^y U_y + S_y^{ib,c} - \nu S_y^{ib,\nu} = 0;$$

$$\begin{aligned} \frac{d}{dt} (M^{xy} \tilde{\psi}) + C^{xy} [\bar{U}^n] \tilde{\psi}^n + S_{xy}^{ib,c,n} [\psi_\infty, \psi^{ib}] - K^{xy} [G_\psi^n] \tilde{\Gamma}_\psi^n - \\ - S_{xy}^v [G_\psi^n, \psi_\infty, \psi^{ib}] - M^{xy} PDA^n = 0. \end{aligned} \quad (13)$$

Here P is the discrete pressure, U_x and U_y are the discrete components of the velocity vector, T_{xy} is the discrete shear Reynolds or subgrid stresses, T_{xx} and T_{yy} are the discrete normal Reynolds or subgrid stresses, $\tilde{\psi}$ is the discrete ψ , $\tilde{\Gamma}_\psi$ is the discrete Γ_ψ ; \bar{U}^{ib} denotes the mass flux arising in case of $\mathbf{v}^{ib} \neq \mathbf{0}$; $S_x^{ib,c}$, $S_x^{ib,\nu}$, $S_y^{ib,c}$, $S_y^{ib,\nu}$, S_{xy}^v are source terms; K^x , K^y and K^{xy} represent the discretization of the diffusive terms; D^x , D^y , D_x^t , D_y^t are the divergence discrete analogues on the corresponding meshes; C^x , C^y and C^{xy} represent the discretization of the convective terms; $G^x = -D_x^t$ and $G^y = -D_y^t$ are the gradient discrete analogues; PDA is the discrete analog of (Prod–Dis + Add); $G_\psi = G^{xy} \tilde{\psi} + S^{ib,g} [\psi_\infty, \psi^{ib}]$ is the discrete analogue of $\partial\psi/\partial x$ and $\partial\psi/\partial y$ which are computed in the middle of $\Omega_{i,j}$ fluid faces.

The time integration of the differential algebraic system (12) is performed with a semi-implicit projection method based on the Adams — Bashforth/second-order

backward differentiation formula (AB/BDF 2) scheme. Predictor step leads to discrete analogues of the Helmholtz equation for velocities prediction \tilde{U}_x , \tilde{U}_y at the time $t_{n+1} = (n+1)\Delta t$:

$$\begin{aligned}
 M_x \frac{3\tilde{U}_x - 4U_x^n + U_x^{n-1}}{2\Delta t} + 2C_x^n U_x^n + 2S_x^{ib,c,n} - C_x^{n-1} U_x^{n-1} - S_x^{ib,c,n-1} - \\
 - D_x^T (P^n - T_{xx}^n) - D_x^{\tau,n} T_{xy}^n - \nu K_x \tilde{U}_x - \nu S_x^{ib,v} = 0; \\
 M_y \frac{3\tilde{U}_y - 4U_y^n + U_y^{n-1}}{2\Delta t} + 2C_y^n U_y^n + 2S_y^{ib,c,n} - C_y^{n-1} U_y^{n-1} - S_y^{ib,c,n-1} - \\
 - D_y^T (P^n - T_{yy}^n) - D_y^{\tau,n} T_{xy}^n - \nu K_y \tilde{U}_y - \nu S_y^{ib,v} = 0.
 \end{aligned} \tag{14}$$

Here Δt is the constant time discretization step. Corrector step is the following:

$$\begin{aligned}
 \frac{3}{2} M_x \frac{U_x^{n+1} - \tilde{U}_x}{\Delta t} - D_x^T (P^{n+1} - P^n) = 0; \quad \frac{3}{2} M_y \frac{U_y^{n+1} - \tilde{U}_y}{\Delta t} - D_y^T (P^{n+1} - P^n) = 0; \\
 D_x U_x^{n+1} + D_y U_y^{n+1} + \bar{U}^{ib,n+1} = 0.
 \end{aligned}$$

It leads to the following discrete analogue of Poisson equation for pressure function $\Phi = 2\Delta t(P^{n+1} - P^n)/3$:

$$A\Phi = D_x \tilde{U}_x + D_y \tilde{U}_y + \bar{U}^{ib,n+1}, \tag{15}$$

$A = -D^x (M^x)^{-1} (D^x)^T - D^y (M^y)^{-1} (D^y)^T$. Then flow variables at the time point t_{n+1} are computed by the following formulae:

$$U_x^{n+1} = \tilde{U}_x + M_x^{-1} D_x^T \Phi; \quad U_y^{n+1} = \tilde{U}_y + M_y^{-1} D_y^T \Phi; \quad P^{n+1} = \frac{3\Phi}{2\Delta t} + P^n. \tag{16}$$

After this, new values of Reynolds or subgrid stresses T_{xx}^{n+1} , T_{yy}^{n+1} , T_{xy}^{n+1} are computed according to (8), (9) by solving the discrete analogues of the equations from the used turbulence model:

$$\begin{aligned}
 M^{xy} \frac{\tilde{\Psi}^{n+1} - \tilde{\Psi}^n}{\Delta t} + C^{xy} [\bar{U}^n] \tilde{\Psi}^n + S_{xy}^{ib,c,n} [\Psi_\infty, \Psi^{ib}] - K^{xy} [G_\Psi^n] \tilde{\Gamma}_\Psi^n - \\
 - S_{xy}^v [G_\Psi^n, \Psi_\infty, \Psi^{ib}] - M^{xy} P D A^n = 0.
 \end{aligned} \tag{17}$$

Numerical experiments. The flow past circular airfoil was simulated using the developed modification of the LS-STAG method. The time averaged drag coefficient C_D and the Strouhal number St were computed. The coefficient C_D was obtained by averaging over a large period of time the unsteady load $C_D(t) = \frac{F_{xa}(t)}{\rho V_\infty^2 / 2}$.

Flow simulation at low Reynolds numbers ($Re < 10^3$). The LS-STAG method allows to receive the results are in good agreement with the experimental and computational data, even on very coarse meshes (Table 3). No turbulence models have been used.

Table 3

Comparison of C_D and St at $Re = 100$ and $Re = 200$ with known experimental and numerical results from the literature

Source	Re = 100		Re = 200	
	C_D	St	C_D	St
Zdravkovich [10] (experiment)	1.21...1.41	0.16...0.17	–	–
LS-STAG (present study, 120×148)	1.31	0.17	1.33	0.20
LS-STAG (present study, 240×204)	1.32	0.17	1.33	0.20
LS-STAG (present study, 480×408)	1.32	0.17	1.33	0.20
Cheny [2] (LS-STAG, 550×350)	1.32	0.17	1.33	0.20
Henderson [11]	1.35	0.16	1.34	0.20
He [12]	1.35	0.17	1.36	0.20

Flow simulation at medium Reynolds numbers ($Re = 10^3 \dots 10^4$). The flow was simulated at the Reynolds numbers $Re = 1000$ (on non-uniform meshes 120×148 with $\Delta t = 5 \cdot 10^{-2}$ and 240×296 with $\Delta t = 10^{-3}$) and $Re = 3900$ (on non-uniform meshes 120×148 with $\Delta t = 10^{-3}$ and 240×296 with $\Delta t = 5 \cdot 10^{-4}$). These values of the Re were chosen because the experimental data [10, 11] and results of other researchers [14–17] are known for them. Computational results are shown in Table 4 and in Fig. 5. These results are in good agreement with experimental data for simulation on coarse meshes by using the proposed modification of the LS-STAG method. But since the considered models works well only at high Reynolds numbers, it is hardly possible to improve the numerical results, for example, by mesh refinement. In our opinion the wall functions usage can be an efficient solution to this problem.

Table 4

Comparison of C_D and St values with known experimental and numerical results

Turbulence model	Number of cells	Re = 1000		Re = 3900	
		C_D	St	C_D	St
Experiment [10]	–	0.98	0.21	0.93	0.22
Experiment [13]	–	1.12	–	1.01	–
Smag., LES, $C_S = 0.1$ [14]	1 103 520	–	–	1.08	–
Smag., LES, $C_S = 0.1$ (spectral) [15]	30 720	–	–	1.01	0.22
Smag., LES, $C_S = 0.1$ (finite volume) [15]	855 040	–	–	1.07	0.24
$k - \varepsilon$, RANS [16]	46 304	1.00	0.15	1.00	0.15
Real $k - \varepsilon$, RANS [16]	46 304	–	0.17	–	0.20
$k - \omega$ SST, RANS [16]	46 304	–	0.23	–	0.25
$k - \varepsilon$, RANS [17], ANSYS	388 550	1.12	–	0.74	–
$k - \omega$ SST, RANS [17], ANSYS	388 550	0.99	–	0.62	–

Turbulence model	Number of cells	Re = 1000		Re = 3900	
		C_D	St	C_D	St
Smag., LES, $C_s = 0.1$ [17], ANSYS	388 550	1.15	0.21	1.07	–
Smag., LES, $\Delta = \Delta^{\max}$, $C_s = 0.2$, present study	71 040	1.35	0.24	1.11	0.26
Smag., LES, $\Delta = \Delta^{\max}$, $C_s = 0.5$, present study	71 040	1.37	0.25	1.10	0.25
S-A, RANS, present study	71 040	1.37	0.25	1.13	0.25
S-A, DES, $C_s = 0.7$, present study	71 040	1.37	0.25	1.11	0.25
$k - \epsilon$, RANS, present study	71 040	1.36	0.25	1.23	0.28
$k - \epsilon$, LES, $\Delta = \Delta^{\max}$, $C_s = 0.9$, present study	71 040	1.37	0.25	1.11	0.25
$k - \omega$, RANS, present study	71 040	1.32	0.24	1.18	0.24
$k - \omega$, DES, $C_s = 1.0$, present study	71 040	1.32	0.25	1.00	0,25
$k - \omega$ SST, RANS, present study	71 040	1.34	0.25	1.14	0.25

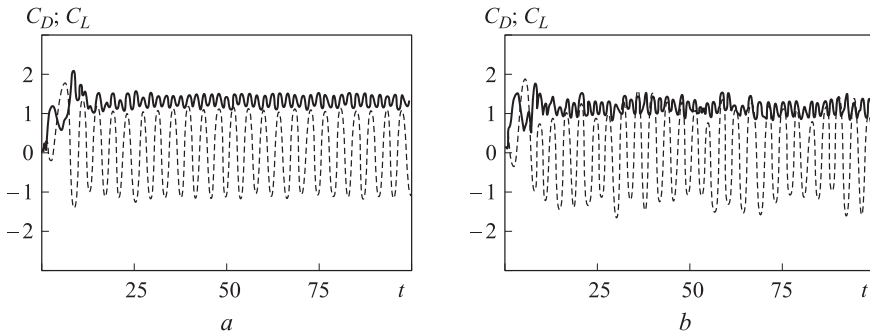


Fig. 5. Computed unsteady load $C_D(t)$ and $C_L(t)$ (RANS, $k - \omega$ model, mesh 240×296):
 a – Re=1000 ; b – Re=3900

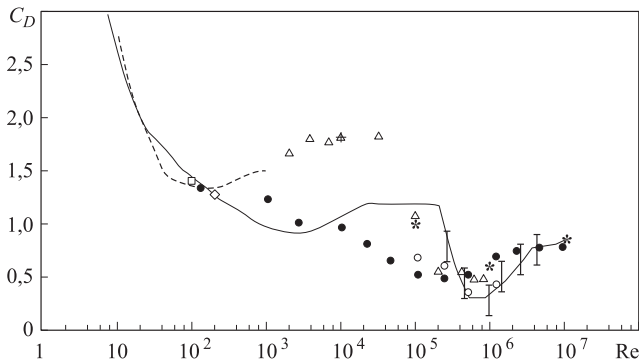


Fig. 6. Comparison of the drag coefficient computed values with experimental [18] and computational data on meshes M1–M5 [19] and [20]:

— Wieselsberger [18]; - - - Henderson, 2D calculations [20]; \diamond — mesh M1; + — mesh M2; \square — mesh M3; \times — mesh M4 with Smagorinsky model; Δ — mesh M4; * — mesh M5; \bullet — LS-STAG ($k - \omega$, RANS, 240×296); \circ — LS-STAG (480×592)

Flow simulation at high Reynolds numbers ($Re = 10^5 \dots 10^7$). The flow was simulated at the Reynolds numbers $Re = 10^5 \dots 10^7$ (on non-uniform meshes 240×296 with $\Delta t = 5 \cdot 10^{-4}$ and 480×592 with $\Delta t = 10^{-4}$). Results obtained on mesh 480×592 are very close to experimental data [18], see Fig. 6. At $Re = 2 \cdot 10^5$, the boundary layer on the cylinder surface undergoes a transition from laminar to turbulent [19]. This transition leads to a delay of the separation of flow from the cylinder surface causing a substantial reduction in the drag force. This is often referred to as "drag crisis". This phenomenon was simulated by using modified LS-STAG immersed boundary method (Fig. 6).

Conclusions. The key points of the LS-STAG method [2, 21] extension for RANS/LES/DES turbulence models were described. For the shear Reynolds stresses and for the eddy viscosity an additional mesh (xy -mesh) is introduced. The general approach to the construction of the LS-STAG discretization for differential equations of the EVM models on the additional xy -mesh shown. The Smagorinsky, Spalart — Allmaras, $k-\varepsilon$, $k-\omega$ and $k-\omega$ SST turbulence models are considered. To validate modified LS-STAG immersed boundary method the flow past a circular airfoil at $Re = 10^2 \dots 10^7$ was simulated. Computational results are in good agreement with established results from the literature. Also, the so-called "drag crisis" phenomenon of circular cylinder at $Re = 10^5 \dots 10^6$ was simulated.

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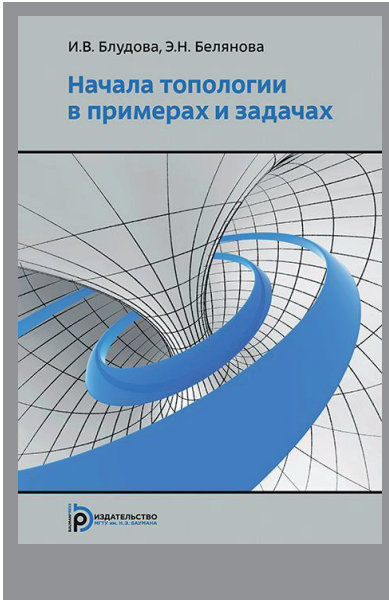
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